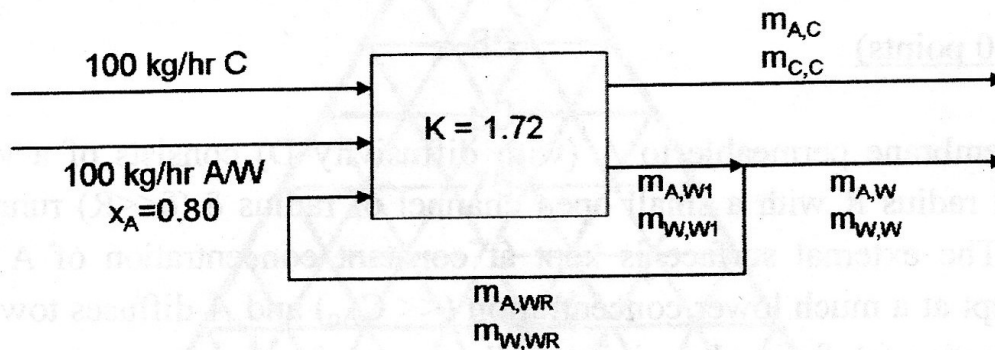


### Problem 3 (30 points)

An extraction process to remove acetone (A) from water (W) involves mixing 100 kg/hr chloroform (C) with 100 kg/hr of an A/W mixture containing 80wt% A at 25°C. A recycle stream sends half of the exiting W/A mixture back into the extractor. W and C are essentially immiscible, and  $K = 1.72$  ( $X_{A,C\text{-Rich Phase}}/X_{A,W\text{-Rich Phase}}$ ) for A/W/C systems at 25°C. The process is depicted below, where unknown mass flow rates are labeled below:



- Set up but do not solve an equation to determine the amount of A extracted into the C phase in kg/hr ( $m_{A,C}$ ). The only variable in the equation should be  $m_{A,C}$ . (12 points)
- If instead of using 100 kg/hr of C, we use 100 kg/hr of methyl isobutyl ketone (MIBK), will we be able to extract more or less acetone from the A/W mixture? (8 points)
- Suppose that unknown amounts of W, A, and MIBK are mixed at 25°C and 1 atm, and the resulting mixture forms two liquid phases in equilibrium.
  - Use Gibbs Phase Rule to determine how many equilibrium mass fractions must be measured in order to determine the rest. (5 points)
  - Use the tertiary phase diagram to justify your answer to part 1 (**in two lines or less**). (5 points)

### Problem 4 (30 points)

An ideal liquid mixture of benzene and n-hexane at 30°C at 1 atm contains 54.5 mol% benzene. The mixture is fed to a heater at a rate of 100 mol/s where it is heated to a temperature of 75°C (and remains at 1 atm). The resulting vapor and liquid phases are in equilibrium and leave the heater as separate streams.

- Calculate the molar flow rates of the vapor and liquid discharge streams. (15 points)
- Calculate the heat supplied by the heater in kW for this process. (15 points)

Assume heat capacities are constant with respect to temperature:

$$(C_P)_{\text{benzene(vapor)}} = 0.0741 \text{ kJ/mol}^\circ\text{C}$$

$$(C_P)_{\text{benzene(liquid)}} = 0.1265 \text{ kJ/mol}^\circ\text{C}$$

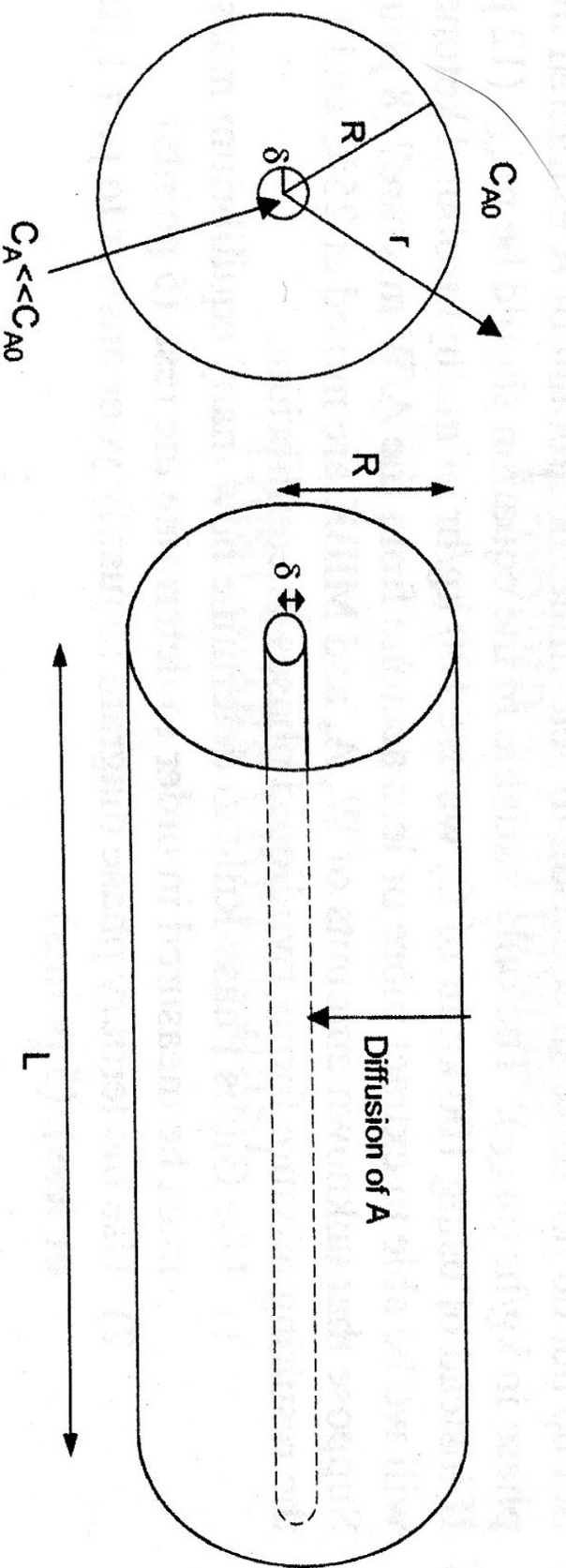
$$(C_P)_{\text{n-hexane(vapor)}} = 0.1374 \text{ kJ/mol}^\circ\text{C}$$

$$(C_P)_{\text{n-hexane(liquid)}} = 0.2163 \text{ kJ/mol}^\circ\text{C}$$

Calculate the compressibility factor,  $Z$ , of superheated steam at 200 bar and 200 °C using the steam tables. Now determine  $z$  for the same conditions using a compressibility chart ( $T_c=347^\circ\text{C}$ ,  $P_c=221.2$  bar). Compare the two values. (20 points)

Problem 2 (20 points)

A porous membrane permeable to A (with diffusivity  $D$ ) consists of a very long cylinder of length  $L$  and radius  $R$  with a small open channel of radius  $\delta$  ( $\delta \ll R$ ) running axially along its centerline. The external surface is kept at constant concentration of A ( $C_{A0}$ ) and the inner channel is kept at a much lower concentration ( $\ll C_{A0}$ ) and A diffuses towards the centerline in the radial direction ( $r$ ), from where it is rapidly removed.



Derive the equation for the diffusion flux of A (molar rate/area) in the radial direction. Solve the