## Question 1: [10 points]

Take both the turbine and the tank as the CV. Since the air entering the turbine has uniform properties, CV analysis gives

1<sup>st</sup> law:  $m_i h_i - W_{out} = m_2 u_2$ since  $m_1=0$  and  $Q_{in}=Q_{out}=0$ with constant Cp and Cv →  $W_{out} = m_i C_p T_i - m_2 C_v T_2$   $m_2=m_i = PV/R_{air}T = 500 \text{ x1 / }(0.287 \text{ x250}) = 6.969 \text{ kg}$  $W_{out} = 6.969 \text{ kg x } (1 \text{ kJ/kg-K x 300K} - 0.713 \text{ kJ/kg-K x 250 K}) = 848.5 \text{ kJ}$ 

## Question 2: [10 points]

- a) The energy of an isolated system must remain constant, but the entropy can only decrease. False, entropy of an isolated system will only stay the same or increase.
- b) The change in entropy of a closed system is the same for any process between two specified states.

True, entropy is a property and independent of process.

- c) The entropy of a fixed amount of an ideal gas increases in every isothermal compression. False, entropy decreases with increasing pressure.
- d) Consider two different sets of reservoirs 1) T<sub>H</sub>=675K, T<sub>L</sub>=325K, 2), T<sub>H</sub>=625K, T<sub>L</sub>=275K. For the Carnot heat engine cycle, setting 1) is better than 2). False, thermal efficiency 1)=51.9% 2)56%
- e) For an ideal gas, its specific internal energy, enthalpy, and entropy depend on temperature only. False. Even for an ideal gas, its specific entropy depends on a second intensive property.

## Question 3: [10 points]

a) The process is steady flow:

$$\dot{W} = \dot{m}(h_2 - h_1) = \dot{m} \cdot c_p (T_2 - T_1)$$
, and  $\eta_c = \frac{h_{2s} - h_1}{h_2 - h_1} = \frac{T_{2s} - T_1}{T_2 - T_1}$ 

for isentropic compression from 100 kPa to 300 kPa,

$$\frac{T_{2s}}{T_1} = \left(\frac{P_2}{P_1}\right)^{(k-1)/k} = \left(\frac{300kPa}{100kPa}\right)^{0.287} = 1.37 \Rightarrow T_1 = 293.15\text{K}, \ T_{2s} = 401.24\text{K},$$
  
From  $\eta_c = \frac{T_{2s} - T_1}{T_2 - T_1}, \ T_2 - T_1 = \frac{T_{2s} - T_1}{\eta_c} \Rightarrow T_2 = T_1 + \frac{T_{2s} - T_1}{\eta_c} = 293.15 + \frac{401.24 - 293.15}{0.85} = 420.32\text{K}$   
 $\dot{W} = \dot{m} \cdot c_p (T_2 - T_1) = 1kg/s \cdot 1 \frac{kJ}{kg \cdot K} (420.32 - 293.15)K = 127.2 \frac{kJ}{s} = 127.2kW$ 

b) Entropy generation between compressor inlet and outlet

$$\Delta s = c_p \ln \frac{T_2}{T_1} - R \ln \frac{P_2}{P_1} = 1 \frac{kJ}{kg \cdot K} \ln \frac{420.32K}{293.15K} - 0.287 \frac{kJ}{kg \cdot K} \ln \frac{300kPa}{100kPa} = 0.045 \frac{kJ}{kg \cdot K}$$

$$Q_H = Q_{sand} = mCdT_H$$
$$\eta_{HE,rev} = 1 - \frac{T_L}{T_H} = \frac{W_{net}}{Q_H}$$

$$\begin{split} W_{net} &= mQ_H \left( 1 - \frac{T_L}{T_H} \right) \\ &= mCdT_H \left( 1 - \frac{T_L}{T_H} \right) \\ &= mC \left( dT_H - \frac{T_L}{T_H} dT_H \right) \\ &= mC \left( \int_{303}^{1273} dT_H - \int_{303}^{1273} \frac{T_L}{T_H} dT_H \right) \\ &= mC(1203 - 303 - T_L(\ln 1273 - \ln 303)) \\ &= mC(970 - 298(1.435)) \\ W_{net} &= 433.8 kJ \end{split}$$

Alternatively, one can consider the net entropy generation is zero  $W_{net} = Q_H - Q_L$   $Q_H = m_{sand} * C * (1000 - 300) = 776 kJ$  $Q_L = -T_L \Delta S_{reservior}$ 

Need to find  $\Delta S_{reservior}$ , we use reversible concept  $\Delta S_{sand} + \Delta S_{reservior} = 0$   $Q_L = T_L \Delta S_{sand}$ ,  $\Delta S_{sand} = m_{sand} C \ln \frac{(1000 + 273)}{30 + 273} = 1.1483kJ/K$   $Q_L = T_L \Delta S_{sand} = 298 * 1.1483kJ/K = 342.199kJ$  $W_{net} = Q_H - Q_L = 776 - 342.199 = 433.801kJ$