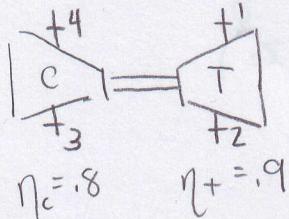


Name Solution

MIDTERM EXAMINATION #2 (11/13/00)

1. In an air turbine/compressor unit, the turbine extracts work from the working fluid and transfer it to the compressor. The air enters the turbine at 500 C, and 2 MPa and exits it at 100 KPa. The air enters the compressor at 20 C and 100 KPa. The kinetic and potential energy through the compressor and turbine can be neglected. Considering that the turbine has an isentropic efficiency of 90% and the compressor of 80%, calculate the pressure at the compressor exit.



$$\text{State 1: } T_1 = 500^\circ\text{C} = 773\text{K}$$

$$P_1 = 2 \text{ MPa}$$

$$\text{State 2: } P_2 = 100 \text{ kPa} \quad \text{For } 800\text{K} \quad k = 1.354$$

$$T_{2,S} = T_1 \left(\frac{P_2}{P_1} \right)^{\frac{k-1}{k}} = 773\text{K} \left(\frac{2000 \text{ kPa}}{100 \text{ kPa}} \right)^{\frac{1.354-1}{1.354}}$$

$$= 1692\text{K}$$

$$\text{iterate: } \frac{773\text{K} + 1692\text{K}}{2} = 1232\text{K} \rightarrow \text{use } k @ 1000\text{K}$$

$$T_{2,D} = 773\text{K} \left(\frac{2000 \text{ kPa}}{1000 \text{ kPa}} \right)^{\frac{1.336-1}{1.336}}$$

$$T_{2,D} = 1642\text{K}$$

$$\text{state 3: } T_3 = 20^\circ\text{C} = 293\text{K}$$

$$P_3 = 100 \text{ kPa}$$

Turbine

$$\vec{W}_{in}^0 + \vec{Q}_{in}^0 + m h_1 = \vec{W}_{out} + \vec{Q}_{out}^0 + m h_2$$

$$\vec{W}_{out} = \frac{m(h_1 - h_2)}{m}$$

$$\vec{W}_{out} = h_1 - h_2 = C_p (T_1 - T_{2,D}) = (1.142)(773\text{K} - 1642) = -992 \text{ kJ}$$

Compressor

$$\eta_t \vec{W}_T = \eta_c \vec{W}_C \rightarrow \frac{\eta_t}{\eta_c} \vec{W}_T - \vec{W}_C = \left(\frac{0.9}{0.8}\right)(992 \text{ kJ}) = 1116 \text{ kJ}$$

$$\vec{W}_{in} + \vec{Q}_{in}^0 + m h_3 = \vec{W}_{out} + \vec{Q}_{out}^0 + m h_4$$

$$\vec{W}_{in} = \frac{m(h_4 - h_3)}{m}$$

$$\vec{W}_{in} = h_4 - h_3 = C_p (T_{4,D} - T_3)$$

(Problem 1 cont.)

$$\frac{W_{in}}{C_p} - T_3 = T_{4,S} = \frac{1116 \text{ kJ}}{1.005} - 293 \text{ K} = 817 \text{ K}$$

$\downarrow C_p \text{ for } 300 \text{ K}$

iterate: $\frac{300 \text{ K} + 817 \text{ K}}{2} = 558.5 \rightarrow \text{use } C_p \text{ for } 550 \text{ K}$

$$T_{4,S} = \frac{1116 \text{ kJ}}{1.040} - 293 \text{ K} = 780 \text{ K}$$

$$\left(\frac{k}{k-1}\right) \frac{T_{4,S}}{T_3} = \left(\frac{P_4}{P_3}\right)^{\frac{k-1}{k}}$$

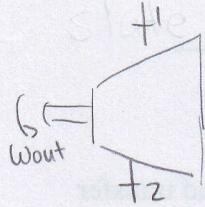
$$\left(\frac{T_{4,S}}{T_3}\right)^{\frac{k}{k-1}} = \frac{P_4}{P_3} \rightarrow P_4 = P_3 \left(\frac{T_{4,S}}{T_3}\right)^{\frac{k}{k-1}} \xrightarrow{\text{cp for } 550 \text{ K}} = (100 \text{ kPa}) \left(\frac{780 \text{ K}}{293 \text{ K}}\right)^{\frac{1.040}{1.040-1}}$$

$$\boxed{P_4 = 11373 \text{ GPa}}$$

2. Steam enters an adiabatic turbine at 7 MPa, 600°C and 80 m/s and leaves at 50 kPa, 150°C, and 140 m/s. If the power output of the turbine is 6 MW, find the following

a) the mass flow rate of the steam flowing through the turbine

b) the isentropic efficiency of the turbine



$$\text{State 1: } \begin{cases} V_1 = 80 \text{ m/s} \\ P_1 = 7 \text{ MPa} \\ T_1 = 600^\circ\text{C} \end{cases} \quad \begin{cases} h_1 = 3650.6 \text{ kJ/kg} \\ s_1 = 7.0910 \text{ kJ/kgK} \end{cases} \quad \text{A-6}$$

$$\text{State 2: } \begin{cases} P_2 = 50 \text{ kPa} \\ T_2 = 150^\circ\text{C} \\ V_2 = 140 \text{ m/s} \end{cases} \quad \begin{cases} h_{2,a} = 2780.2 \text{ kJ/kg} \\ s_{2,a} = 7.9413 \text{ kJ/kgK} \end{cases} \quad \text{A-6}$$

a) Find \dot{m}

$$\dot{Q}_{in}^0 + \dot{W}_{in}^0 + \dot{m}(h_1 + \frac{V_1^2}{2} + gZ_1^0) = \dot{Q}_{out}^0 + \dot{W}_{out} + \dot{m}(h_2 + \frac{V_2^2}{2} + gZ_2^0)$$

$$\dot{m}(h_1 + \frac{V_1^2}{2}) = \dot{W}_{out} + \dot{m}(h_2 + \frac{V_2^2}{2})$$

$$\dot{m}(h_1 + \frac{V_1^2}{2} - h_2 - \frac{V_2^2}{2}) = \dot{W}_{out}$$

$$\dot{m} = \frac{\dot{W}_{out}}{(h_1 - h_2 + \frac{V_1^2}{2} - \frac{V_2^2}{2})} = \frac{6000 \text{ kW}}{(3650.6 \text{ kJ/kg} - 2780.2 \text{ kJ/kg} + \frac{(80^2 \text{ m/s} - 140^2 \text{ m/s})}{2} \cdot \frac{1 \text{ kJ/kg}}{1000 \text{ m}^2/\text{s}^2})}$$

$$\boxed{\dot{m} = 6.95 \text{ kg/s}}$$

b) Find η_T

$$\eta_T = \frac{W_a}{W_s}$$

$$\text{State 2 (isentropic): } \begin{cases} P_2 = 50 \text{ kPa} \\ s_1 = s_2 \end{cases} \quad x_{2s} = \frac{s_{2s} - s_f}{s_{fg}}$$

$$x_{2s} = \frac{7.0910 - 1.0912}{6.5019} = .9228$$

$$\dot{Q}_{in}^0 + \dot{W}_{in}^0 + \dot{m}(h_1 + \frac{V_1^2}{2} + gZ_1^0) = \dot{Q}_{out}^0 + \dot{W}_{out} + \dot{m}(h_{2s} + \frac{V_2^2}{2} + gZ_2^0)$$

$$\dot{W}_{out,s} = \dot{m}(h_1 - h_{2s} + \frac{V_1^2 - V_2^2}{2})$$

$$h_{2s} = h_f + x_{2s} h_{fg}$$

$$= 340.54 + (.9228)(2304.7)$$

$$h_{2s} = 2467.3 \text{ kJ/kg}$$

$$\dot{W}_{out,s} = (6.95 \text{ kg/s})(3650.6 \text{ kJ/kg} - 2467.3 \text{ kJ/kg} + \frac{80^2 \text{ m/s} - 140^2 \text{ m/s}}{2} \cdot \frac{1 \text{ kJ/kg}}{1000 \text{ m}^2/\text{s}^2})$$

$$\dot{W}_{out,s} = 8178 \text{ kJ}$$

$$\eta_T = \frac{W_a}{W_s} = \frac{6000 \text{ kJ}}{8178 \text{ kJ}} = \boxed{0.73}$$